

# Numerical Simulation Approaches for Modeling Natural Gas Hydrate Systems in Geologic Media Subject to Geomechanical Stresses

March 12, 2019

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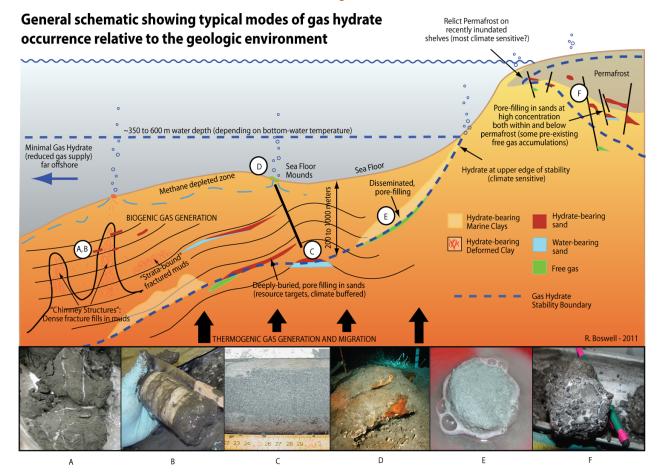
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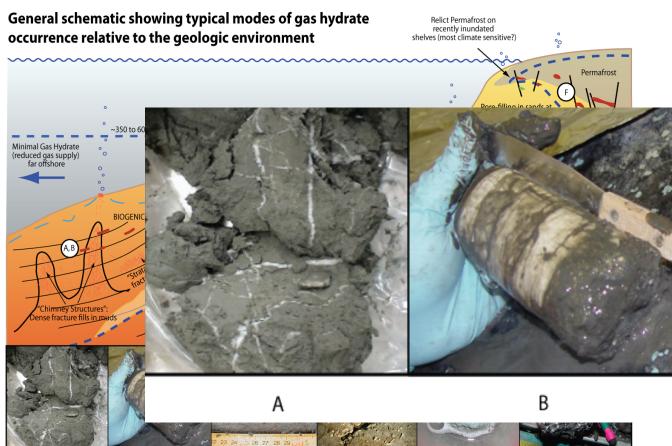
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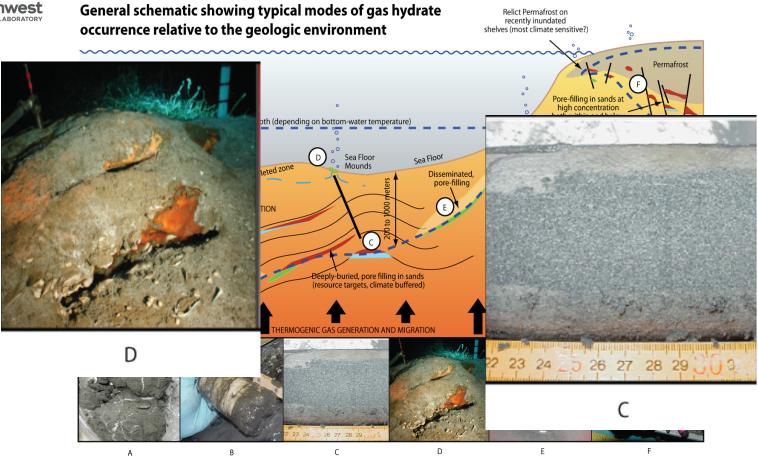




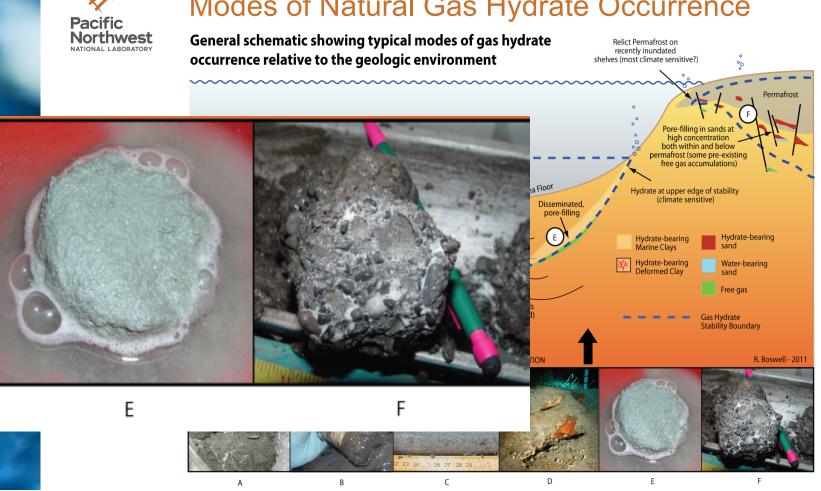






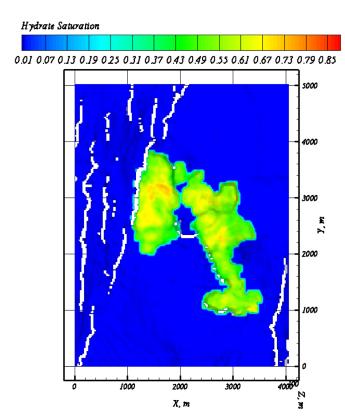


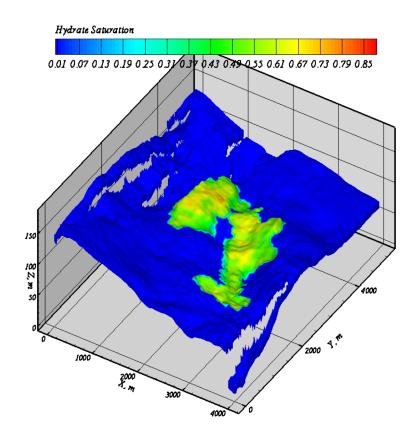






### Gas Hydrate Systems: Hydrate Distributions on the Alaska Northslope





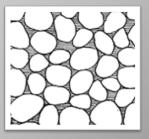


### Challenges in Modeling Natural Gas Hydrates in Geologic Environments

- Hydrate Thermodynamics
- Heat Transport
- Mobile and Immobile Phases
- Relative Permeability Saturation Capillary Pressure
- Kinetic Hydrate Dissolution Formation
- Kinetic Exchange of Guest Molecules
- Potential for Three-Phase Hydraulics
- Phase Appearances Disappearances Transitions
- Coupled Geomechanics
- Hydrate Dependent Mechanical Properties
- Hydrate Dependent Porosity and Permeability
- Nonlinearities Abound
- Phase Equilibria

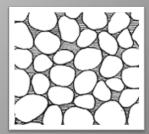
#### Pore Space Occupancy

Aqueous
Gas
Nonaqueous Liquid
Gas Hydrate
Ice



#### **Hydrate-Matrix Structure**

Encrustration
Cementation
Matrix-Supporting
Pore-Filling





### An International Effort to Compare Gas Hydrate Reservoir Simulators: IGHCCS1

- Five benchmark and field-scale problems focused on gas hydrate production via depressurization and thermal stimulation
- Proceedings of the 6th International Conference on Gas Hydrates (ICGH 2008), Vancouver, British Columbia, Canada, July 6-10, 2008.
- 11 International Participants
  - University of Akron
  - Lawrence Berkeley National Laboratory
  - National Energy Technology Laboratory
  - University of West Virginia
  - U.S. Geological Survey
  - Ryder Scott Company, Petroleum Consultants
  - Japan Oil Engineering Company, Ltd.
  - National Institute of Advanced Industrial Science and Technology
  - Pacific Northwest National Laboratory
  - University of Tokyo
  - Fekete Associates Inc.



Photo: Bill Lawson

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### 2<sup>nd</sup> International Gas Hydrate Code Comparison Study: IGHCCS2

- Five benchmark and challenge problems focused on gas hydrate production via depressurization and thermal stimulation with geomechanical coupling
- Principal Investigators
  - Mark White, Pacific Northwest National Laboratory
  - Tim Kneafsey, Lawrence Berkeley National Laboratory
  - Yongkoo Seol, National Energy Technology Laboratory
- 23 International Participants
- Problem Champions
- NETL EDX System
- Regularly scheduled teleconferences for code descriptions, problem development, solution comparisons, and scientific discussions
- Current focus on benchmark problems





#### 2<sup>nd</sup> International Gas Hydrate Code Comparison Study: IGHCCS2





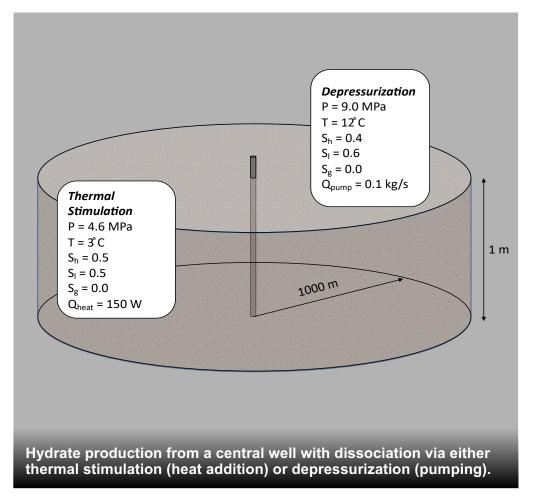
# Benchmark Problem 1 Similarity Solutions: Hydrate Dissociation in a Radial Domain

#### **Problem Champion**

Mark White<sup>1,\*</sup>

<sup>1</sup>Pacific Northwest National Laboratory

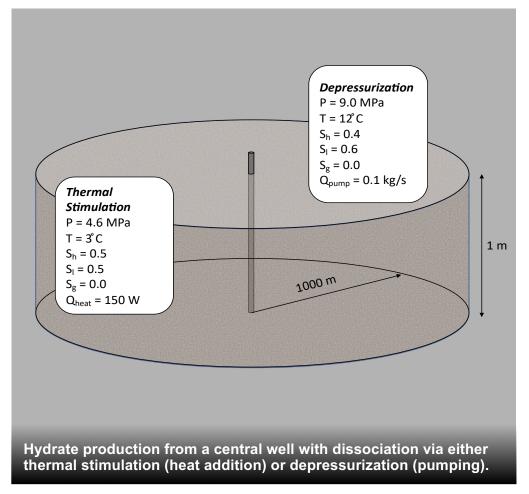
\*mark.white@pnnl.gov





#### **Problem Notes**

- Similarity solution
- No geomechanics
- 1D radial flow
- Fine discretization near well
- Secondary hydrate formation away from well
- No ice formation
- Two-phase pumping during depressurization





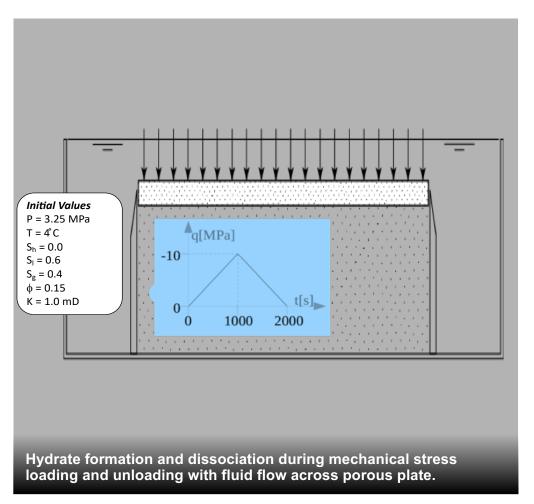
#### Benchmark Problem 2 Extended Terzaghi Problem

#### **Problem Champion**

Shubhangi Gupta<sup>1,\*</sup>

<sup>1</sup>GEOMAR Helmholtz Center for Ocean Research Kiel

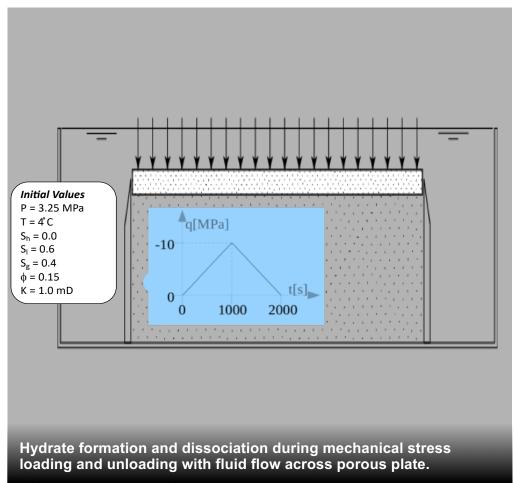
\*sgupta@geomar.de





#### **Problem Notes**

- 1D vertical domain
- Coupled flow, heat transport, thermodynamics, and geomechanics
- Without hydrate formation via higher initial temperature
- Variation with hydrate saturation dependent shear modulus
- Variation with rapid hydrate formation/dissociation kinetics





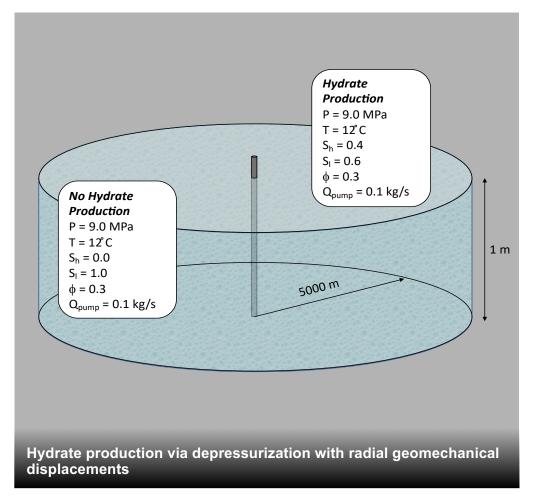
### Benchmark Problem 3 Radial Production

#### **Problem Champions**

Matthew Reagan<sup>1,\*</sup>
Alejandro Queiruga<sup>1</sup>

<sup>1</sup>Lawrence Berkeley National Laboratory

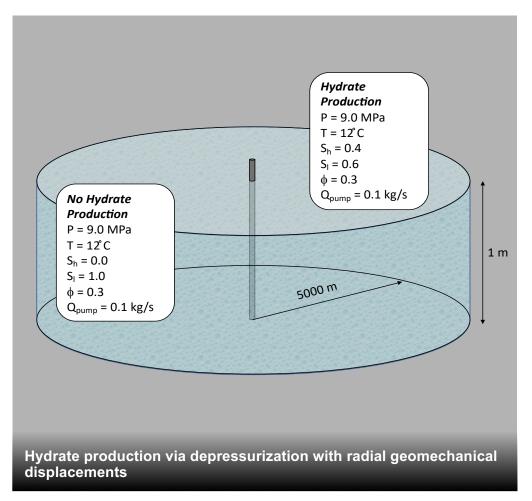
\*mtreagan@lbl.gov





#### **Problem Notes**

- Radially symmetric domain
- No hydrate production
  - Coupled flow and geomechanics
  - Comparison to analytical solution
- Hydrate production
  - Coupled flow and geomechanics
  - No analytical solution
- Constant traction on top
- Rollers on bottom





#### Benchmark Problem 4 Nankai Trough

#### **Problem Champions**

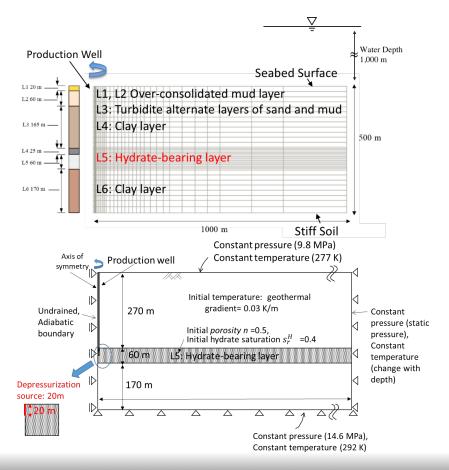
Sayuri Kimoto<sup>1,\*</sup>

Catherine Yonkofski<sup>2</sup>

<sup>1</sup>Kyoto University

<sup>2</sup>Pacific Northwest National Laboratory

\*kimoto.sayuri.6u@kyotou.ac.jp

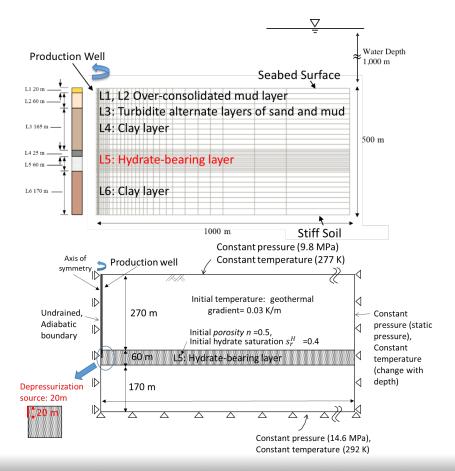


Hydrate production via depressurization from gas hydrate bearing sediments in the Nankai Trough, Japan



#### **Problem Notes**

- 2D radially symmetric domain
- 6 sediment layers with 1 hydrate-bearing layer
- Water depth of 1,000 m
- Shear modulus dependent on hydrate saturation
- Production yields vertical displacements
- Initial geothermal, vertical effective stress, and horizontal effective stress gradients



Hydrate production via depressurization from gas hydrate bearing sediments in the Nankai Trough, Japan



# Benchmark Problem 5 Isotropic Consolidation with Hydrate Dissociation

#### **Problem Champions**

Shun Uchida<sup>1,2,\*</sup>

Xuerui Gai<sup>1</sup>

Jeen-Shang Li<sup>1,3</sup>

Eugene Myshakin<sup>1</sup>

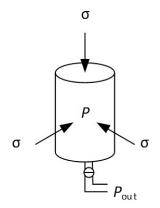
Yongkoo Seol<sup>1</sup>

<sup>1</sup>NETL

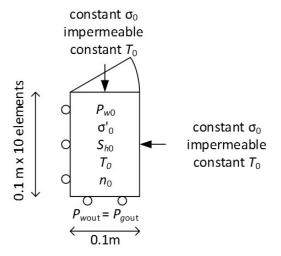
<sup>2</sup>Rensselaer Polytechnic

<sup>3</sup>University of Pittsburgh

\*uchids@rpi.edu



- σ is constant throughout.
- Initial P is larger than P<sub>out</sub>.
- Open the valve and let pore water drain.
- With time, P reaches to P<sub>out</sub>.
- Volume of water out = soil volume reduction

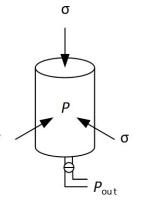


Depressurization induces isotropic consolidation, leading to volumetric deformation

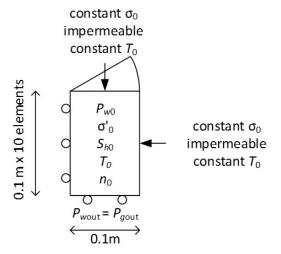


#### **Problem Notes**

- Axisymmetric domain with 10 ogrid cells/elements
- Important to know how each hydrate simulator handles volumetric deformation as well as hydrate dissociation
- To see how each simulator couples flow and volumetric deformation
- To see how each simulator couples hydrate dissociation and deformation



- σ is constant throughout.
- Initial P is larger than P<sub>out</sub>.
- · Open the valve and let pore water drain.
- With time, P reaches to P<sub>out</sub>.
- Volume of water out = soil volume reduction



Depressurization induces isotropic consolidation, leading to volumetric deformation



#### Coupled THMC Modeling Approach in STOMP-HYDT-KE



Conservation of mobile component mass

$$\begin{split} &\frac{\partial}{\partial t} \int\limits_{V_{n}} \left[ \sum_{\gamma = l, n, g} \left( \phi \; \rho_{\gamma} \; s_{\gamma} \; \omega_{\gamma}^{i} \right) \right] dV_{n} = \int\limits_{\Gamma_{n}} \left[ \mathbf{F}^{i} \bullet \mathbf{n} \right] d\Gamma_{n} + \int\limits_{V_{n}} \left[ \sum_{\gamma = l, n, g} \left( \omega_{\gamma}^{i} \; m_{\gamma} \right) \right] dV_{n} \\ &\int\limits_{V_{n}} \left[ \sum_{\gamma = l, n, g} -K_{e} \; M^{i} \; A_{h} \left( \varphi_{m}^{i} - \varphi_{h}^{i} \right) - \left\{ K_{f} \; \varphi_{m}^{i} \; M^{i} \; A_{h} \left( P_{m}^{v} - P_{h}^{v} \right) / \; P \; for \; P_{m}^{v} > P_{h}^{v} \right\} \; \right] dV_{n}; \; for \; i = CH_{4}, CO_{2}, N_{2} \end{split}$$

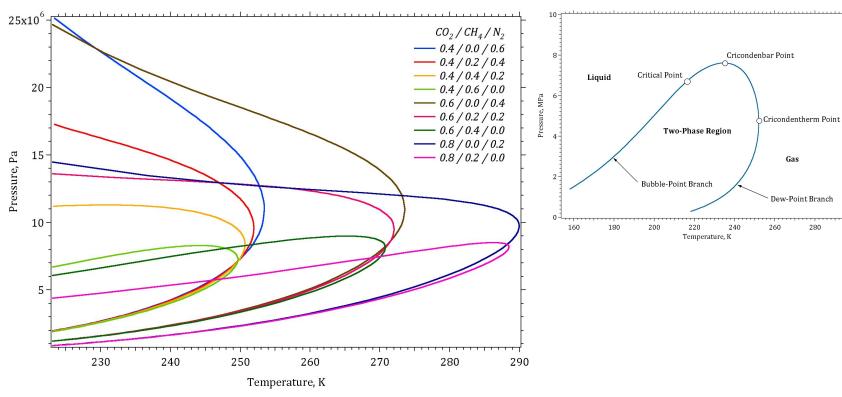
Conservation of hydrate component mass

$$\begin{split} &\frac{\partial}{\partial t} \int\limits_{V_{n}} \left[ \phi \; \rho_{h} \; s_{h} \; \omega_{h}^{i} \right] dV_{n} = \\ &\int\limits_{V_{n}} \left[ K_{e} \; M^{i} \; A_{h} \left( \varphi_{m}^{i} - \varphi_{h}^{i} \right) + \left\{ K_{f} \; \varphi_{m}^{i} \; M^{i} \; A_{h} \left( P_{m}^{v} - P_{h}^{v} \right) / \; P \; for \; P_{m}^{v} > P_{h}^{v} \right\} \right] dV_{n}; \; for \; i = CH_{4}, CO_{2}, N_{2} \end{split}$$



#### **Equation of State Phase** Envelopes for the Mobile Phases



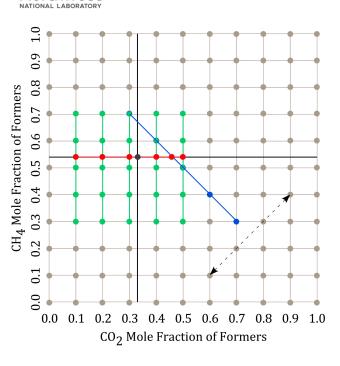


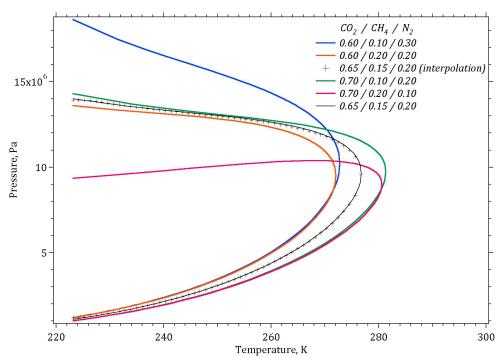
Gas



#### **Tabular Interpolation Scheme**







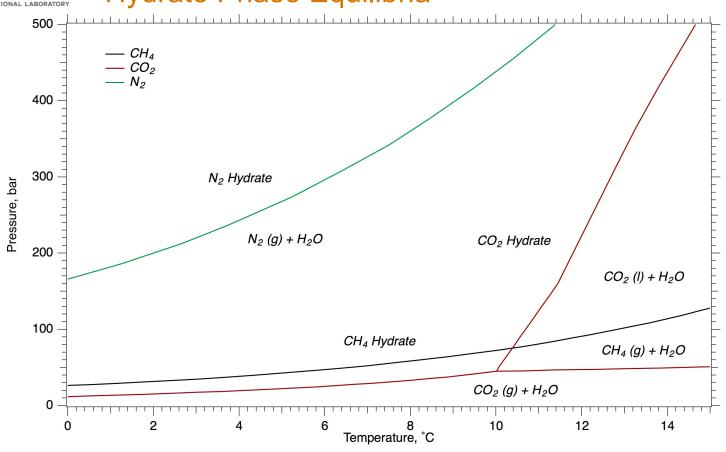
$$T_{tab} = T_{tab}^{cricondentherm} \left[ \frac{T}{T_{mix}^{cricondentherm}} \right] for \ T < T_{mixture}^{cricondentherm}$$

$$for \ T < T_{mixture}^{cricondentherm} \qquad P_{tab} = P \left[ \frac{P_{tab}^{upper} - P_{tab}^{lower}}{P_{mix}^{upper} - P_{mix}^{lower}} \right] + P_{tab}^{lower} \quad for \ P_{mix}^{lower} < P < P_{mix}^{upper}$$



#### Gas Hydrate Systems – Hydrate Phase Equilibria

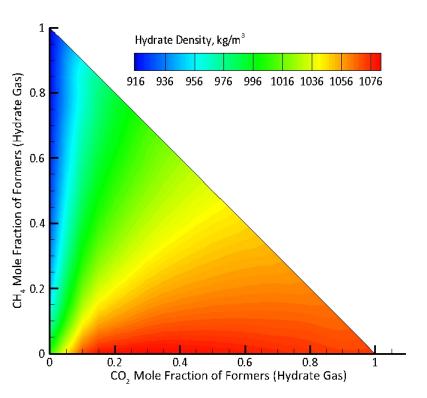


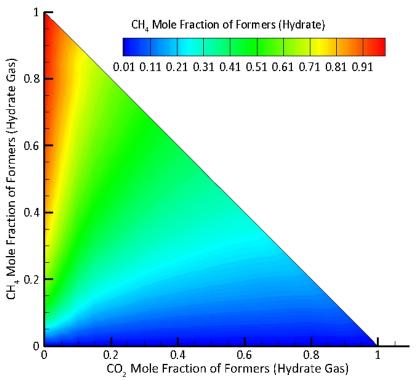




### Gas Hydrate Systems – Ternary Hydrate Properties from Tables











Phase Condition #10 Series $s_h = 0.0, s_n + s_g = 0.0, s_\ell + s_i = 1.0$			
Energy	T	Temperature	
Water Mass	P	Pressure	
Mobile CO <sub>2</sub> Mass	$P_v^{CO_2}$	CO <sub>2</sub> Vapor Pressure	
Mobile CH <sub>4</sub> Mass	$P_v^{CH_4}$	CH <sub>4</sub> Vapor Pressure	
Mobile N <sub>2</sub> Mass	$P_v^{N_2}$	N <sub>2</sub> Vapor Pressure	
Hydrate CO <sub>2</sub> Mass	$M_h^{CO_2}$	Hydrate CO <sub>2</sub> Mass	
Hydrate CH <sub>4</sub> Mass	$M_h^{CH_4}$	Hydrate CO <sub>2</sub> Mass	
Hydrate N <sub>2</sub> Mass	$M_h^{N_2}$	Hydrate CO <sub>2</sub> Mass	
Salt	$\mathcal{Y}_{\ell}^{\mathcal{S}}$	Brine Mass Fraction of Total Salt	





Energy	T	Temperature
Water Mass	$s_{\ell} + s_{i}$	Aqueous + Ice Saturation
Mobile CO <sub>2</sub> Mass	$z_m^{CO_2}$ or $P$	CO <sub>2</sub> Mole Fraction or Pressure
Mobile CH <sub>4</sub> Mass	$z_m^{CH_4}$ or $P$	CH <sub>4</sub> Mole Fraction or Pressure
Mobile N <sub>2</sub> Mass	$z_m^{N_2}$ or $P$	N <sub>2</sub> Mole Fraction or Pressure
Hydrate CO <sub>2</sub> Mass	$M_h^{CO_2}$	Hydrate CO <sub>2</sub> Mass
Hydrate CH <sub>4</sub> Mass	$M_h^{CH_4}$	Hydrate CO <sub>2</sub> Mass
Hydrate N <sub>2</sub> Mass	$M_h^{N_2}$	Hydrate CO <sub>2</sub> Mass
Salt	$\mathcal{Y}_{\ell}^{\mathcal{S}}$	Brine Mass Fraction of Total Salt





#### Phase Condition #30 Series $s_h > 0.0, s_n + s_g > 0.0, s_\ell + s_i < 1.0$

Energy	T	Temperature
Water Mass	$s_{\ell} + s_{i}$	Aqueous + Ice Saturation
Mobile CO <sub>2</sub> Mass	$z_m^{CO_2}$ or $P$	CO <sub>2</sub> Mole Fraction or Pressure
Mobile CH <sub>4</sub> Mass	$z_m^{CH_4}$ or $P$	CH <sub>4</sub> Mole Fraction or Pressure
Mobile N <sub>2</sub> Mass	$z_m^{N_2}$ or $P$	N <sub>2</sub> Mole Fraction or Pressure
Hydrate CO <sub>2</sub> Mass	$\varphi_h^{CO_2}$ or $s_h$	CO <sub>2</sub> Mole Fraction of Former
Hydrate CH <sub>4</sub> Mass	$arphi_h^{\mathit{CH}_4}$ or $s_h$	CH <sub>4</sub> Mole Fraction of Former
Hydrate N <sub>2</sub> Mass	$arphi_h^{N_2}$ or $s_h$	N <sub>2</sub> Mole Fraction of Former
Salt	$\mathcal{Y}_{\ell}^{\mathcal{S}}$	Brine Mass Fraction of Total Salt





Energy Temperature Water Mass Pressure Mobile CO<sub>2</sub> Mass CO<sub>2</sub> Vapor Pressure  $P_{v}^{CH_{4}}$ Mobile CH<sub>4</sub> Mass CH₄ Vapor Pressure  $P_{\nu}^{N_2}$ Mobile N<sub>2</sub> Mass N<sub>2</sub> Vapor Pressure  $\varphi_h^{CO_2}$  or  $s_h$  CO<sub>2</sub> Mole Fraction of Former Hydrate CO<sub>2</sub> Mass  $\varphi_h^{CH_4}$  or  $s_h$  CH<sub>4</sub> Mole Fraction of Former Hydrate CH<sub>4</sub> Mass  $\varphi_h^{N_2}$  or  $s_h$  N<sub>2</sub> Mole Fraction of Former Hydrate N<sub>2</sub> Mass  $y_{\ell}^{s}$ **Brine Mass Fraction of Total Salt** Salt



#### Gas Hydrate Systems - Phase **Transition Example**





Phase Condition #10 Series 
$$s_h = 0.0, s_n + s_g = 0.0, s_{\ell} + s_i = 1.0$$

- Assume a hydrate phase exists (common approach!)
- Compute a hydrate equilibrium pressure  $P_h^{eq} = func[T, \varphi_h^{CO_2}, \varphi_h^{CH_4}, \varphi_h^{N_2}]$
- Compute the vapor pressure of formers  $P_{\nu} = P_{\nu}^{CO_2} + P_{\nu}^{CH_4} + P_{\nu}^{N_2}$
- Compute the total gas pressure  $P_q = P_v^{CO_2} + P_v^{CH_4} + P_v^{N_2} + P_v^{H_2O}$
- $if(P_v > P_h^{eq})$  then hydrate forms
- $if(P_a > P_\ell + P_{entrv})$  then nonaqueous gas or liquid forms

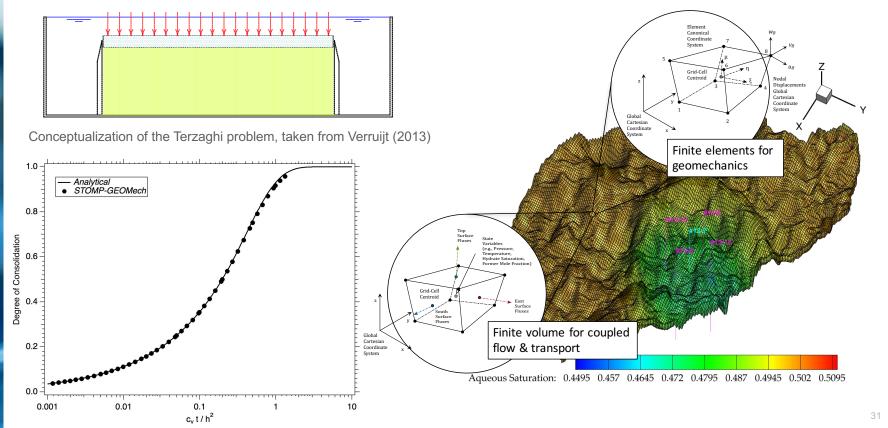


Phase Condition #30 Series  $s_h > 0.0, s_n + s_a > 0.0, s_\ell + s_i < 1.0$ 



### Coupling Flow and Transport with Poro-Thermo-Elastic Geomechanics







#### **Fixed Stress Sequential Coupling**



#### Flow and Transport Solution via Finite Volume

- Iterative Solution of Governing Equations for Flow and Transport
- Effective Permeability Function of Flow Porosity  $\phi_{flow}$  and  $s_h$
- Yielding Pore Pressure  $P_{pore}$  and Temperature T

#### Poro-Thermo-Elastic Geomechanics via Finite Element

- Direct Solution of the Governing Equations for Geomechanics
- Compute the Mechanical Porosity  $\phi_{mech}$
- $\phi_{mech}^{k+1} = func \left[\phi_{mech}^{k}, \Delta P_{pore}, \Delta \varepsilon_{V}\right]$
- $if \left\{ \frac{\phi_{flow} \phi_{mech}^{k+1}}{\phi_{mech}^{k+1}} > tol (e.g. 10^{-6}) \right\}$



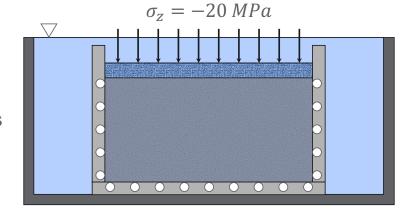


Upper Fluid Boundary
Conditions  $T = 4^{\circ}C$ 

P = 3.0 MPa

 $s_h = 0.0, s_\ell = 1.0$ 

Side Mechanical Boundary Conditions  $u_x = 0.0 m$ 



**Upper Mechanical** 

**Boundary Conditions** 

Side Fluid Boundary Conditions  $T = 10^{\circ}C$ no flow

**Initial Conditions** 

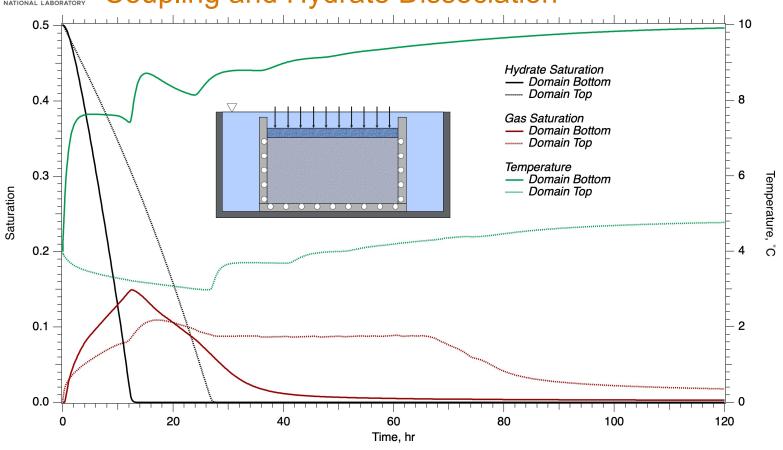
 $state\ conditions = equilibrium$ 

$$T = 4^{\circ}C$$
  
 $P = 5.0 MPa$   
 $s_h = 0.5, s_{\ell} = 0.5$   
 $\psi_h^{CO_2} = 0.0, \psi_h^{CH_4} = 1.0, \psi_h^{N_2} = 0.0$ 

Bottom Mechanical Boundary Conditions  $u_z = 0.0 m$ 

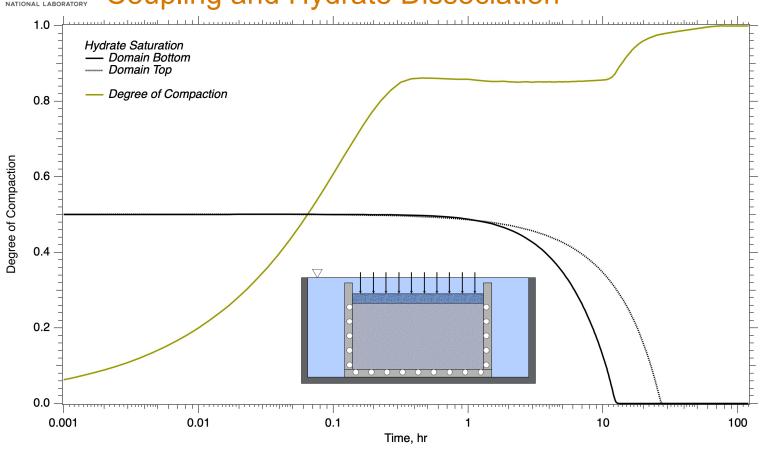






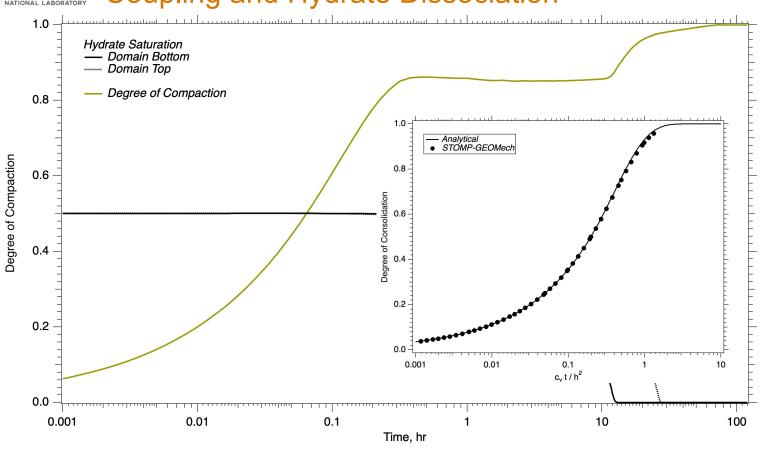














### Thank you

